School of Engineering and Sustainable Development
Institute of Energy and Sustainable Development



# PERFORMANCE MONITORING OF A LARGE UNIVERSITY GSHP SYSTEM

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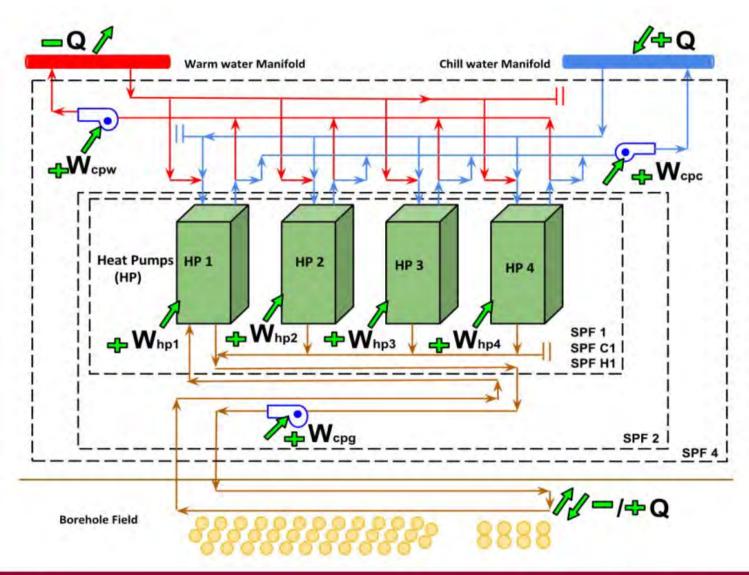
# THE HUGH ASTON BUILDING

- A multi-use building (15,607 m<sup>2)</sup>
- Monitored since opening in Jan 2010
- GSHP system provides all AHU and FCU cooling (360 kW peak) and all underfloor heating (330 kW peak capacity)
- Has Four Water Furnace 2-stage reversible heat pumps
- 56 x 100m deep borehole heat exchangers, 125mm diameter.
   30 l/s peak flow



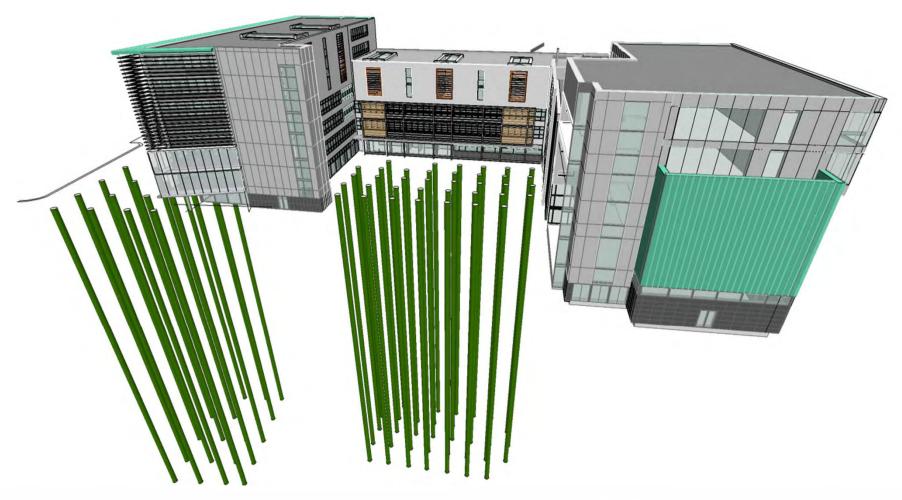


# **SYSTEM SCHEMATIC**





# **BOREHOLE ARRAY DESIGN**



19 + 37 arrays



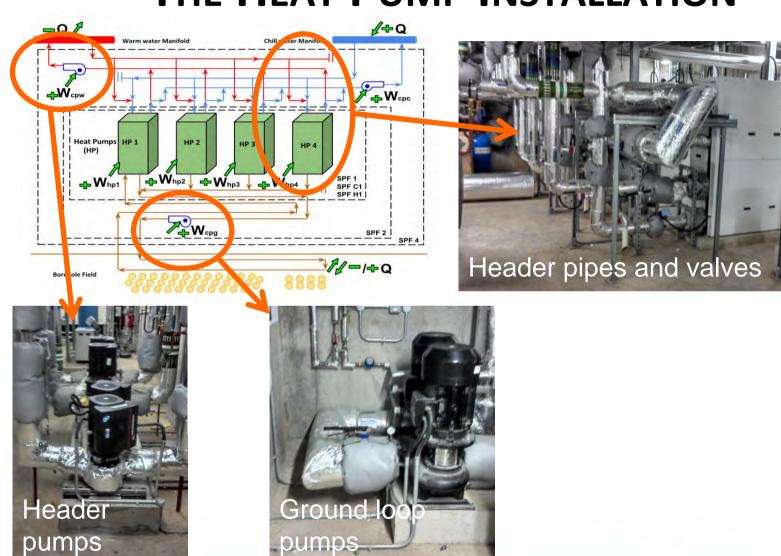
# THE HEAT PUMP INSTALLATION



2-stage design with scroll compressors and plate heat exchangers. Any HP can be used for heating or cooling



# THE HEAT PUMP INSTALLATION





# **MONITORING**

- Aims
  - Performance analysis
  - Reference data sets for model development
- Measurements
  - Ground TRT test analysis
  - Heat pump electrical demand (sub-meters)
  - Ground loop and heating/cooling temperatures and flow rates at 1 minute intervals
  - Borehole temperatures
  - Flow and source/load temperatures for one heat pump
  - BMS Data: compressor operation
- Careful calibration means SPF calculated to +/- 2.7%

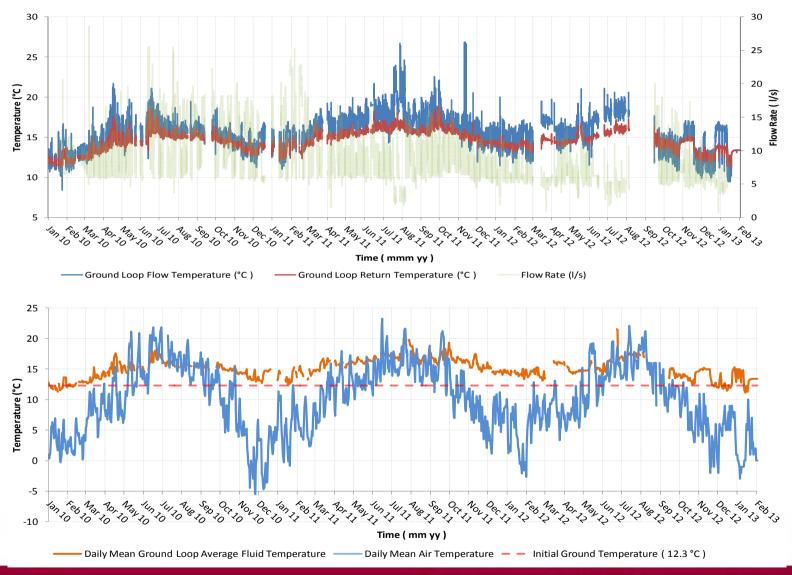


# **MONITORING OUTPUTS**

- Seasonal performance factors (various timescales): SPF1, SPF2, SPF4 for heating/cooling modes
- Ground loop temperature and flow reference data
- Analysis: reasons for heat pump and overall system good/poor performance

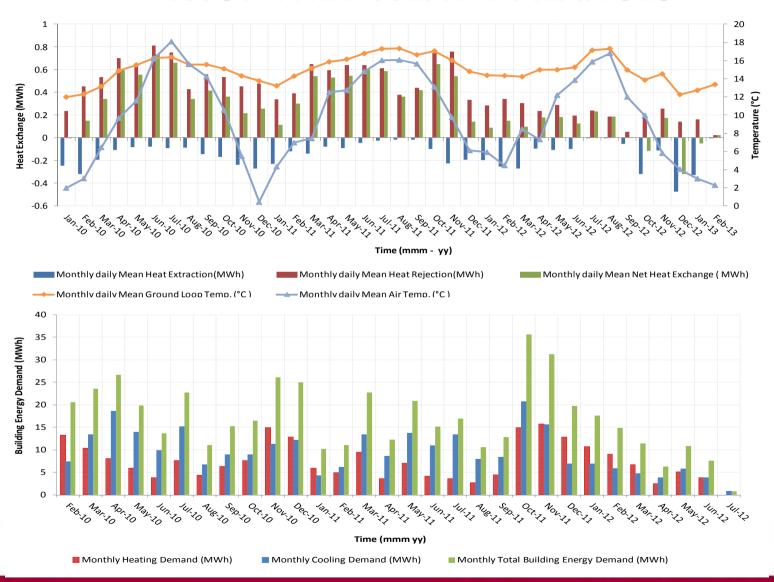


# **GROUND HEAT EXCHANGER PERFORMANCE**



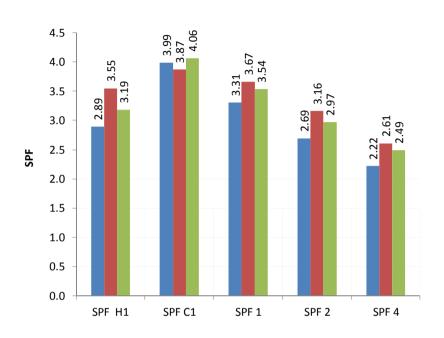


# **MONTHLY HEAT BALANCES**





# SYSTEM EFFICIENCIES



■ May -2010 to April -2011 ■ May -2011 to April -2012 ■ Feb -2010 to July -2012

- Seasonal performance Factors:
  - SPF1 is heat pump alone
  - SPF2 includes the ground loop pump demand
  - SPF 4 includes the heating/cooling header pumps
- RES Directive requires SPFH2 > 2.5

| Year ( Season)           | SPF <sub>H1</sub> | SPF <sub>C1</sub> | SPF <sub>1</sub> | SPF <sub>2</sub> | SPF <sub>4</sub> |
|--------------------------|-------------------|-------------------|------------------|------------------|------------------|
| May -2010 to April -2011 | 2.89              | 3.99              | 3.31             | 2.69             | 2.22             |
| May -2011 to April -2012 | 3.55              | 3.87              | 3.67             | 3.16             | 2.61             |
| Feb -2010 to July -2012  | 3.19              | 4.06              | 3.54             | 2.97             | 2.49             |



# **SYSTEM EFFICIENCIES**

### Questions:

- Are the heat pumps performing as the manufacturers stated?
- What are the main contributors to differences between heat pump and overall system performance?
- What could be done to improve performance?

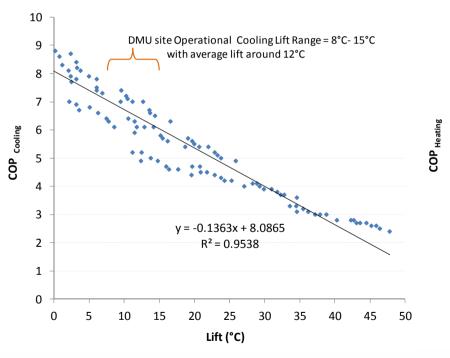
### Approach:

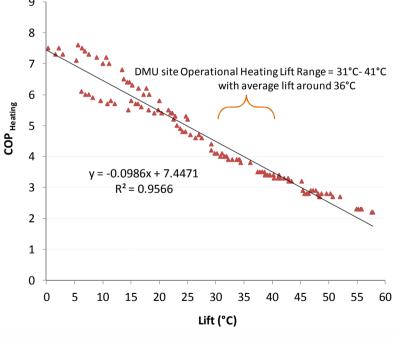
- Compare individual heat pump performance and catalogue data
- Evaluate circulating pump energies
- Examine dynamic operation and control



# **HEAT PUMP EFFICIENCIES**

Heat pump performance varies according to flow rates and inlet temperatures at both load and source-side heat exchangers. Also glycol properties.







# **Heat Pump Performance**

- Most catalogue data shows performance with water.
   20% polypropylene glycol reduces heat transfer by 9% for cooling and 4% for heating in our case.
- We can construct a 'curve fit' model using the corrected catalogue data and predict outputs based on measured fluid temperatures and flow rates.

$$\frac{Q_L}{Q_{L,ref}} = A1 + A2 \left[ \frac{T_{L,in}}{T_{ref}} \right] + A3 \left[ \frac{T_{S,in}}{T_{ref}} \right] + A4 \left[ \frac{V_L}{V_{L,ref}} \right] + A5 \left[ \frac{V_S}{V_{S,ref}} \right]$$

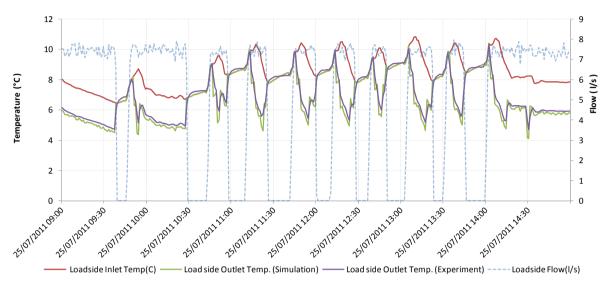
$$\frac{P}{P_{ref}} = B1 + B2 \left[ \frac{T_{L,in}}{T_{ref}} \right] + B3 \left[ \frac{T_{S,in}}{T_{ref}} \right] + B4 \left[ \frac{V_L}{V_{L,ref}} \right] + B5 \left[ \frac{V_S}{V_{S,ref}} \right]$$

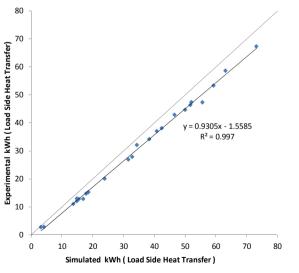
$$y = 1x + 3E \cdot 06$$

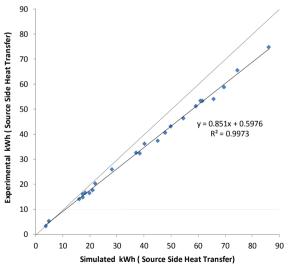
$$R^2 = 0.9953$$

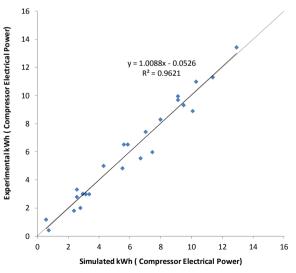
$$y = 100 \quad 150 \quad 200 \quad 250$$
Simulated Cooling Capacity (kw)
$$y = 1 \times 3E \cdot 06 \quad 100 \quad 150 \quad 200 \quad 250 \quad 300$$
Simulated Heat Rejection (kW)

# **HEAT PUMP PERFORMANCE**





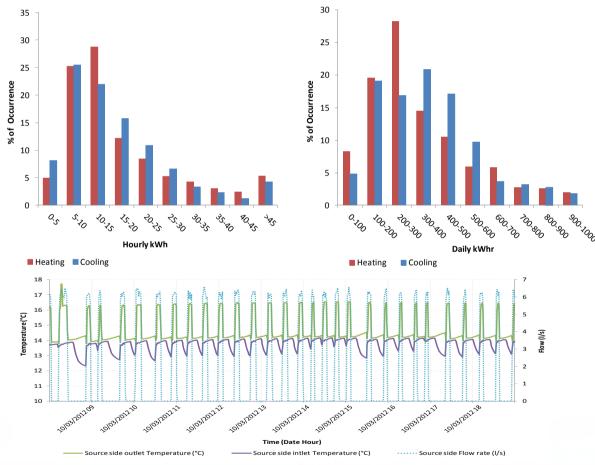






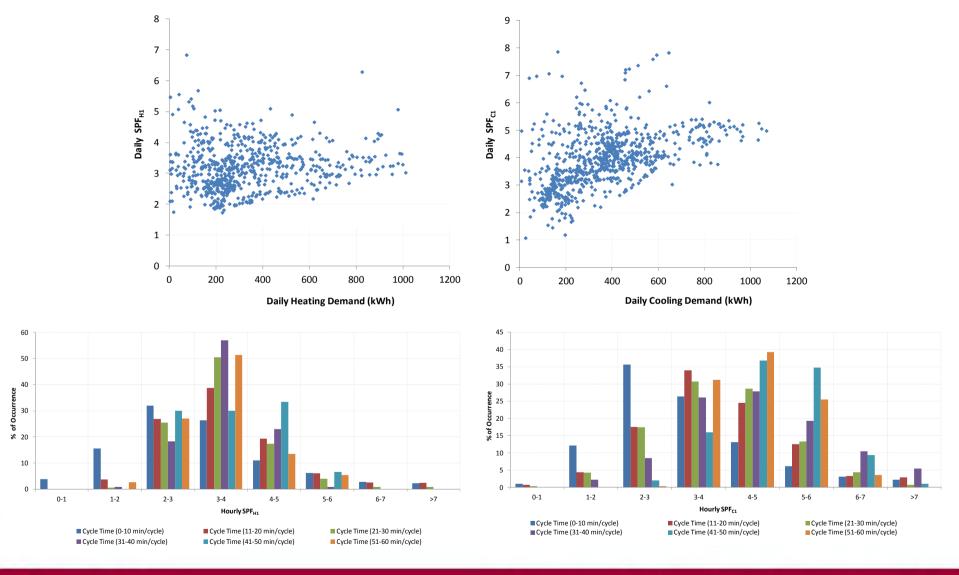
# **DYNAMIC OPERATION**

Only one compressor stage is needed for much of the time. On/off control leads to short cycle times.





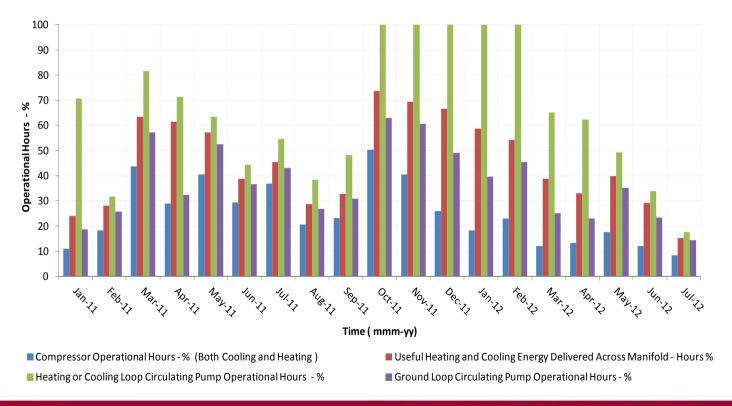
# **DYNAMIC OPERATION**





# **CIRCULATING PUMP OPERATION**

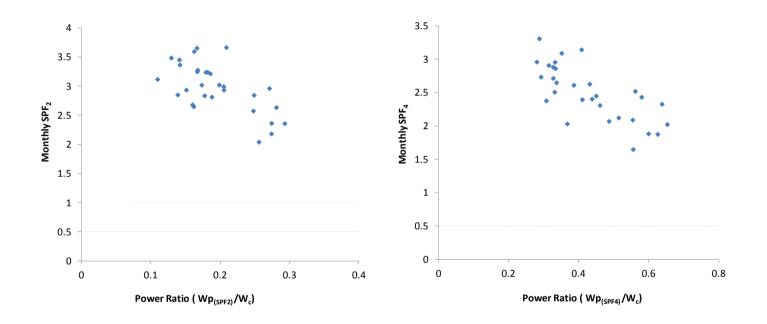
- Pump sizes are large relative to compressor sizes
- Pumps also operate unnecessarily valve, flow switch and control faults





# **CIRCULATING PUMP ENERGY DEMANDS**

Pump demands have a big effect on SPF<sub>2</sub> and SPF<sub>4</sub>



Monthly Pump to Compressor Power Ratio Vs Monthly SPF2, SPF4



## **IMPROVING PERFORMANCE**

- Cycle times would be improved by
  - Smaller lead machine
  - Variable compressor speed
  - Buffer tanks
- Lift could be reduced by heating temperature tuning/reduction
- Pump energy demands could be reduced by:
  - Better hydraulic design
  - More robust control (fault detection/correction)
  - Reduced start-up/shut-down running
  - Ground loop demand control



# **CONCLUSIONS**

- Overall performance satisfactory
- Good ground heat exchanger performance
- Potential improvement:
  - Longer cycle times
  - More resilient control
  - Heating temperature optimization
  - Lower glycol levels
- General lessons:
  - Pump energy, heating temperatures and controls are issues limiting efficiency: as in domestic systems
  - Short timescale dynamics are important
  - Better control integration (design/contract stages) and post installation care are needed

